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## Reactive rimming flow of non-Newtonian fluids

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## ABSTRACT

The steady and non-steady flows of a liquid polymer treated as a non-Newtonian fluid on the inner surface of a horizontal rotating cylinder are investigated. Since the Reynolds number is small and the liquid film is thin, a simple lubrication approximation is applied. Governing equations for non-steady Power-Law and Ellis fluids are solved numerically and the time of transition from non-steady to steady-state mode for various model parameters and flow conditions are defined. The stabilization effect of a chemical reaction within the polymeric fluid (reactive flow) is examined.

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## 1. Introduction

The problem of rotational flow on the inner and/or outer wall of a hollow horizontal cylinder has been of interest for many years due to its wide range of applications in industry [1,2]. Moffatt [3] was the first to derive the condition for the maximal supportable load for a Newtonian liquid. Preziosi and Joseph [4] later presented the same result in another form and named it a run-off condition for coating and rimming flows.

The possible instability of the liquid film on a cylindrical surface is one the most challenging aspects of this problem. The highly unstable nature of rimming Newtonian flow was discussed in a number of publications [5–11]. Although the aforementioned investigations highlight the main characteristics of rimming flow, not enough has been done to show the effect of non-Newtonian properties on such flow, given its importance. Only a few attempts have been made. The power-law [12], Carreau–Yasuda [13], Ellis [14,15], Bingham [16], and viscoelastic models [17,18] have been used to study rimming flow. Fomin et al. [13,14] and Fomin [15] recently extended the estimates, originally made by Moffatt [3] for Newtonian fluids, for a generalized Newtonian fluid. Most polymeric solutes used in rotational coating are non-Newtonian liquids, which exhibit shear-thinning behavior for moderate to high shear rates. Liquid polymers behave as Newtonian liquids near the free surface (at very low shear rates) and exhibit non-Newtonian characteristics above a certain transitional shear rate,  $\dot{\gamma}_t$ . The importance of non-Newtonian effects for generalized Newtonian fluids is characterized by the shear-thinning number  $Wi = \lambda\Omega/\delta$ , where  $\Omega$  is the characteristic angular velocity of the rotating cylinder,  $\delta$  is the ratio of the characteristic thickness of the film and the radius of the cylinder, and  $\lambda \approx (\dot{\gamma}_t)^{-1}$  is a typical time scale for liquid polymers, which is well documented [19] and normally stays in the interval of  $(10^{-2}, 10^{-1})$  seconds. In some situations, e.g. a higher speed of rotation, a thinner liquid layer, or a smaller transition shear rate, the value of  $Wi$  can be quite large. This illustrates the dominating role of non-Newtonian effects. Results of numerical computations available in [13] show that a Carreau fluid exhibits power-law behavior for large values of  $Wi$ . For instance, with  $Wi = 8$ , the results obtained with the Carreau and power-law models practically

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